

### AMENDMENTS TO THE CLAIMS

1. **(Original)** A method for purifying albumin comprising a step of submitting an aqueous albumin solution, with a concentration of 15 g/L to 80 g/L and a pH not lower than 7, to a nanofiltration in a temperature range of 15°C to 55°C.
2. **(Original)** A method according to Claim 1, characterised in that the nanofiltration is carried out on qualified filters having porosities of at least 13 nm.
3. **(Original)** A method according to one of Claims 1 and 2, characterised in that the pH of the aqueous albumin solution is in the range of 7.8 to 11.5, and preferably, of 9 to 10.5.
4. **(Previously presented)** A method according to Claim 1, characterised in that it further comprises a step of adding a pharmaceutically acceptable salt or salt mixture to the aqueous albumin solution to provide a solution with a ionic strength in the range of 0.01 to 0.55.
5. **(Original)** A method according to Claim 4, characterised in that the pharmaceutically acceptable salt is a salt of an alkali metal.
6. **(Original)** A method according to Claim 5, characterised in that the salt of an alkali metal is sodium chloride present in an amount imparting to the albumin solution an ionic strength of 0.15.
7. **(Previously presented)** A method according to Claim 1, characterised in that the concentration of the aqueous albumin solution is in the range of 40 g/L to 60 g/L.
8. **(Previously presented)** A method according to Claim 1, characterised in that the temperature of the aqueous albumin solution is between 30°C and 55°C.

9. **(Previously presented)** A method according to Claim 1, characterised in that the nanofiltration of the aqueous albumin solution is carried out in two successive steps on two filters with decreasing porosities, respectively.
10. **(Currently Amended)** A method according to Claim 9, characterised in that the two successive nanofiltration steps are carried out on filters with porosities of 23 to 50 nm and 15 to 20 nm, respectively.
11. **(Previously presented)** A method according to Claim 1, characterised in that it is implemented with regenerated cellulose filters of 15 nm having a surface area of 0,01 m<sup>2</sup>, at a pressure not exceeding 1 bar.
12. **(Original)** A method according to Claim 11, characterised in that the pressure is in the range of 0.2 to 0.8 bar.
13. **(Previously presented)** A method according to Claim 1, characterised in that the albumin is obtained by ethanol extraction and by purification by ion-exchange or affinity chromatography.
14. **(Previously presented)** A method according to Claim 1, characterised in that it comprises a subsequent step of processing the aqueous albumin solution to make it suitable to a therapeutic use.
- 15.-29. **(Cancelled)**
30. **(Currently Amended)** A virally safe aqueous albumin solution produced by a process that comprises

a) submitting an aqueous albumin solution, with a concentration of 15 g/L to 80 g/L and a pH not lower than 7, to a nanofiltration in a temperature range of 15°C to 55°C, to produce a purified albumin composition; and  
b) adding an alkali metal salt or salt mixture to the purified albumin composition to provide a solution with a ionic strength in the range of 0.01 to 0.55; ~~The virally safe aqueous albumin solution according to Claim 29, wherein said nanofiltration is carried out in two successive steps on two filters with decreasing porosities~~the two successive nanofiltration steps are carried out on filters with porosities of 23 to 50 nm and 15 to 20 nm, respectively.

31. **(Previously Presented)** A virally safe aqueous albumin solution produced by a process that comprises
- a) submitting an aqueous albumin solution, with a concentration of 15 g/L to 80 g/L and a pH between 9 and 10.5, to nanofiltration in a temperature range of 15°C to 55°C, to produce a purified albumin composition; and
  - b) adding sodium chloride to the purified albumin composition to provide a solution with a ionic strength in the range of 0.01 to 0.55; wherein said nanofiltration is carried out in two successive steps on two filters with decreasing porosities of 23 to 50 nm and 15 to 20 nm, respectively; and wherein said process does not comprise the use of polyethyleneglycol or organic salts.